

Masses at Massillon: IFAS for Industrial Loads and Nutrient Removal

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Agenda

- Project Background
 - ▶ Ex. Plant
 - ▶ Future Limits
- Facilities Planning
 - ▶ TP Removal Study
- Transition from Study to Design
 - ▶ *Challenges Arise!*
- Industrial v. In Plant Solutions
- Final Design Challenges
- Summary & Questions

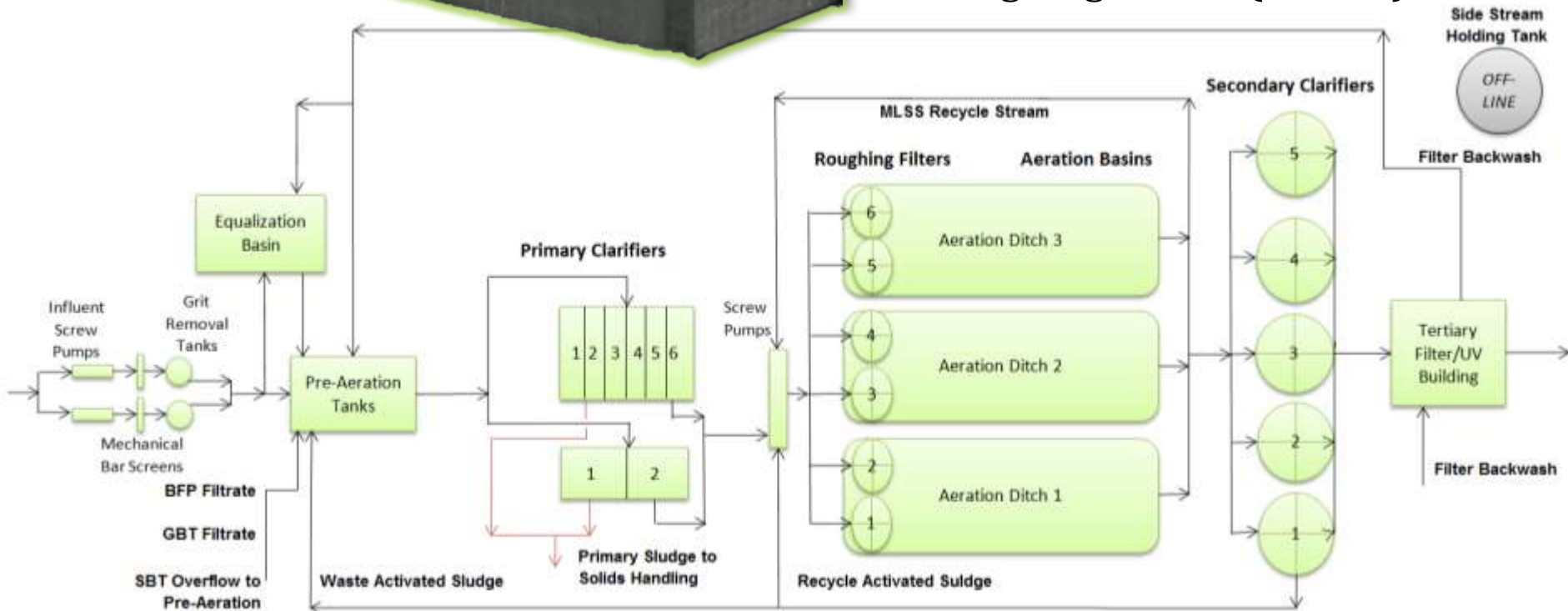


Massillon Ohio WWTP – Ex. Liquid Stream



■ 15.8 MGD Design ADF

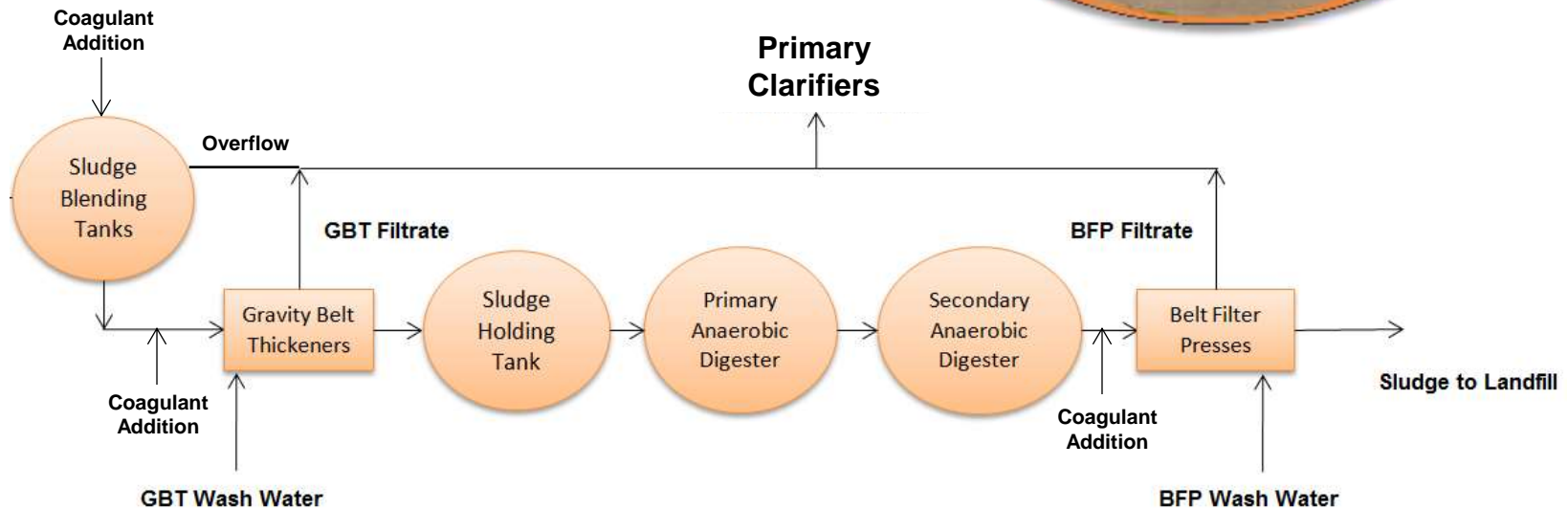
- ▶ Secondary Biological Treatment
 - CBOD₅/Summer NH₃-N
- ▶ Aeration Ditches
- ▶ Roughing Filters (odors?)



Massillon Ohio WWTP – Ex. Solids Treatment

■ Stabilization - Anaerobic Digestion

- ▶ Sludge Blending
- ▶ Gravity Belt Thickening
- ▶ Belt Filter Press Dewatering
- ▶ Coagulant Feed for odor control



Massillon Ohio WWTP – Ex. NPDES Permit

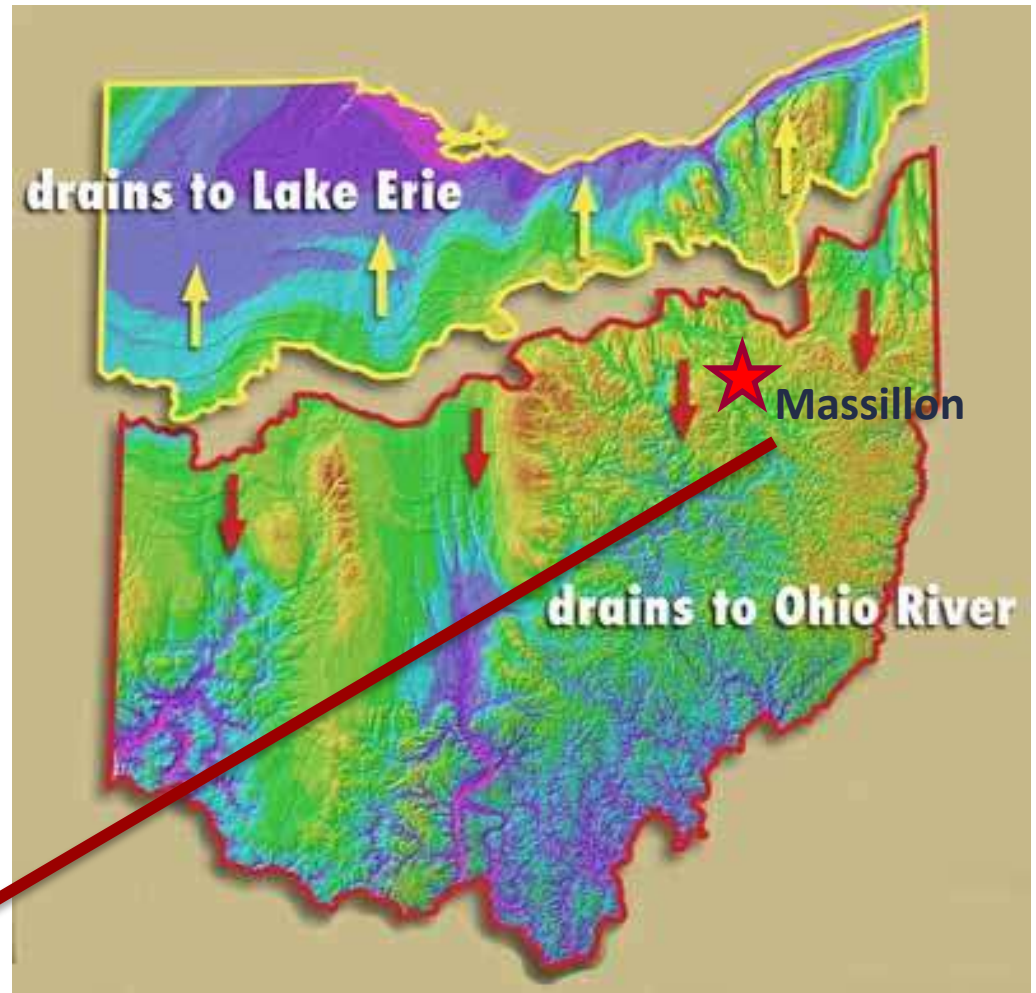
Ex. NPDES Discharge Permit Limitations			
Parameter:		Concentrations- mg/L	
		Weekly	Monthly
TSS		18	12
NH ₃ -N	Summer	2.1	1.4
CBOD ₅	Summer	15	10
	Winter	33	22
TP*		1.5	1.0
*60 mo. after effective date (March 2016)			

- Effective: March 2011
- Expiration: January 2015
 - ▶ Ex. Plant meets TSS, CBOD₅ and NH₃-N
 - ▶ *Improvements required for TP removal – Other improvements?*



Ohio EPA – Nutrient Removal Strategy

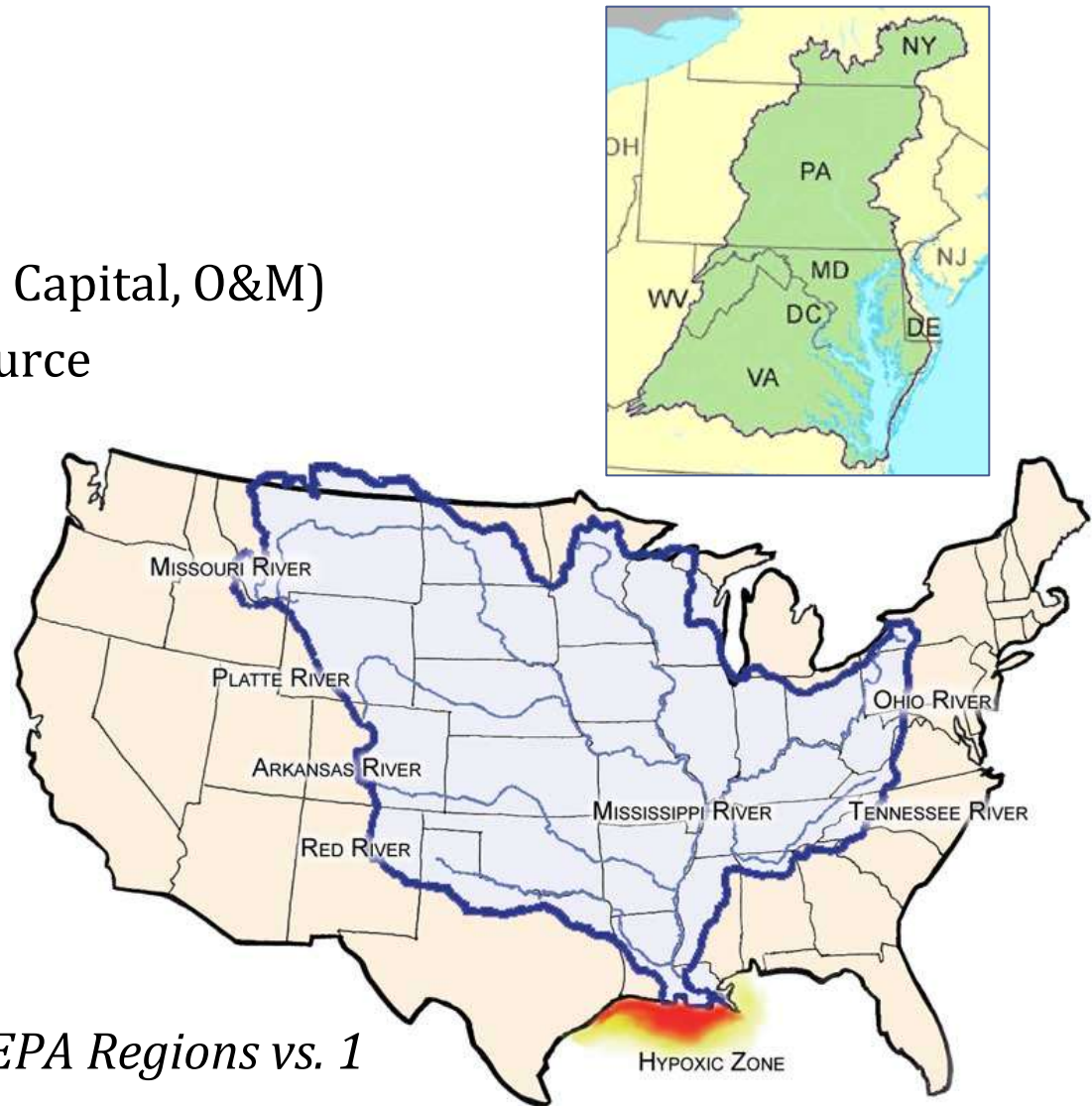
- State Wide Nutrient Reduction Strategy
- TMDLs, watershed plans
- Priority watersheds
- Phase in Effluent Phosphorus (P) limits
- Ohio River Watersheds
 - ▶ State Waters
 - ▶ *Gulf Hypoxia Program*



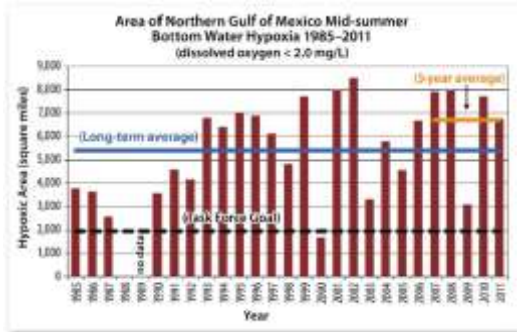
**drains to Mississippi
River Basin**

Gulf Hypoxia Program - may look a lot like Chesapeake Bay's

- Precedence
 - ▶ Science, Regulations
 - ▶ Performance Results
 - › Point Source (TP, TN; Capital, O&M)
 - › (Some) Non-Point Source
 - ▶ Trading
 - ▶ Integrated Planning
 - ▶ Nutrient Recovery
- Policies & Procedures
- Lessons Learned
 - ▶ Fairness
 - ▶ Funding?
 - ▶ Flexibility
 - ▶ *33 vs. 6 States, Multiple EPA Regions vs. 1*



Gulf of Mexico Hypoxia & Pending Nutrient Removal Program



Nutrient Removal (NR) Levels (mg/L)

Biological NR (BNR) – 8-10 TN, 1 TP

Advanced NR (ANR) – 5 TN, 0.5 TP

Enhanced NR (ENR) – 3 TN, 0.1-0.3 TP

Likely Future Effluent Limits?

Massillon WWTP – Improvements Project Goals

- Expansion to 17 MGD
- Pending 1 mg/L TP
 - *Future 10 mg/L TN?*
 - Evaluate BNR
- Take roughing filters offline
 - Odor complaints
- Maintain Existing:
 - Tankage
 - Anaerobic Digestion
 - Industrial Pretreatment
- Facility Plan Update (CTI) and TP Removal Study (OBG)



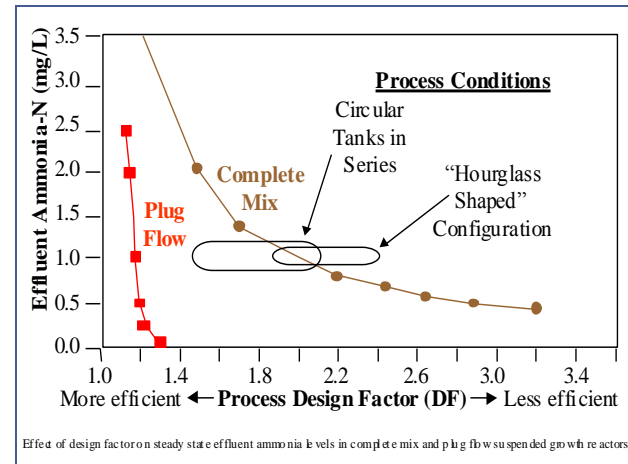
TP Removal Study – Establishing Design Loadings

Current Data				
Parameters	Units	Industrial Load	Calculated Domestic	Measured Plant Influent (2007-2011)
Average Daily Flow	MGD	0.816	9.5	10.3
BOD ₅	mg/L	787	155	205
TSS		309	149	162
Ortho-P		19	0.7	1.2
Total P		17	1.5	2.8
20 Year Prediction				
		Industrial Load	Calculated Domestic	Calculated Future Influent
Design Flow	MGD	2.185	14.8	17
BOD ₅	mg/L	433	155	191
TSS		329	149	173
Ortho-P		19	0.7	1.6
Total P		18	1.5	3.6

- Four Significant Industrial Users (SIUs)
 - ▶ Reported current data, 20 year projections
- Design TP → 3.6 mg/L

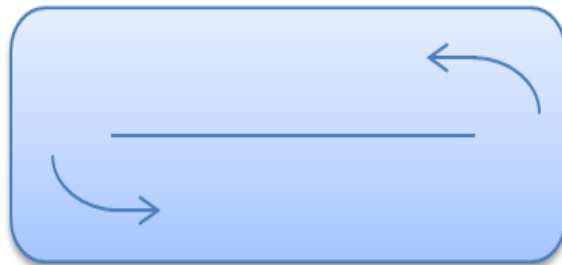
TP Removal Study - Initial Design Ideas

- Remove Roughing Filters
- Three Expansion Options:
 1. Keep Existing Ditch Operations
 2. Convert Ditches to Plug Flow
 3. Convert Ditches to Plug Flow and Add Media (IFAS)



AnoxKaldnes K5 Media

Existing Operations

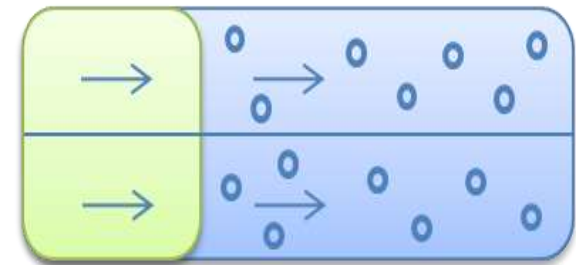


Plug Flow



Anaerobic/Anoxic Zone

Plug Flow with IFAS

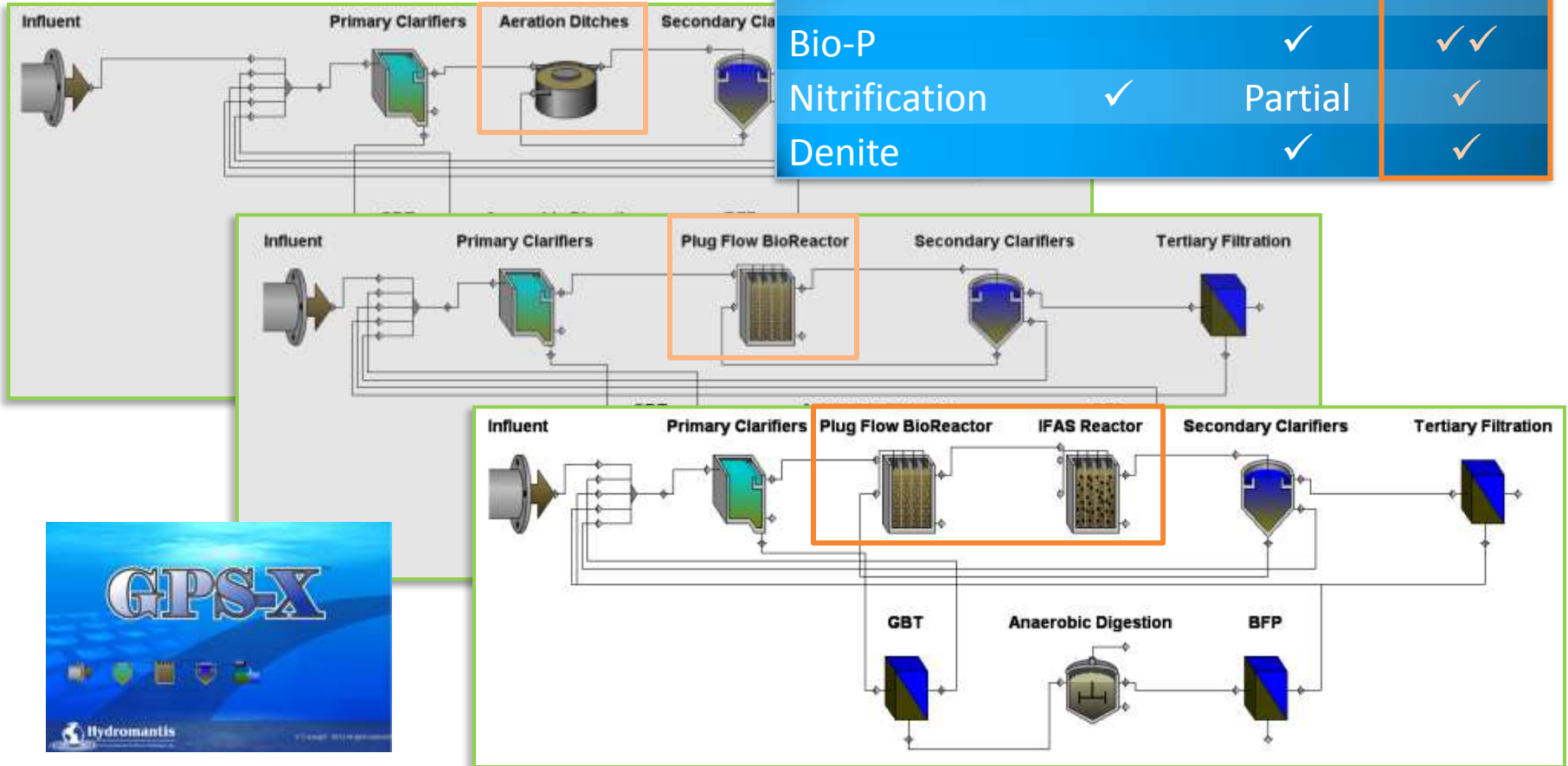


TP Removal Study - Initial Modeling Results

■ Plug Flow + IFAS

- ▶ Predicts best overall treatment

Treatment Achieved	Aeration Ditches	Plug Flow	Plug Flow + IFAS
BOD	✓	✓	✓
Bio-P		✓	✓✓
Nitrification	✓	Partial	✓
Denite		✓	✓



TP Removal Study - Recommendation

Plug Flow + IFAS

Capacity Expansion + Moderate BNR

- Bio-P primary design goal

O+M Savings

- Maintain existing footprint
- An/Ax Zone as selector:
 - Reduce aeration, filamentous growth
 - Improve settling



Facilities Plan Update (& TP Study) - Recommendations

Headworks

- Odor control modifications
- Fine screening

Secondary Treatment

- Demo screw pumps (High DOs)
 - New VTSH Primary Effluent Pump Station (PEPS)
- Conversion of Ditches to Plug Flow + IFAS

Tertiary Treatment

- Replace Ex. Tertiary Filters

Ancillary Upgrades

- Power
- Replace Boilers

Estimated Cost: \$21.6 Million

Transition from Study to Design Phase – *Challenges Arise*

Vendor Review - Limited An/Ax?

- Min Temp: TP *or* TN Removal – not both

City requests TN as Primary Goal

- \$2 M for IR, Ax Volume – \$23.6 M New Total

Time to detail scope and secure 0% loan

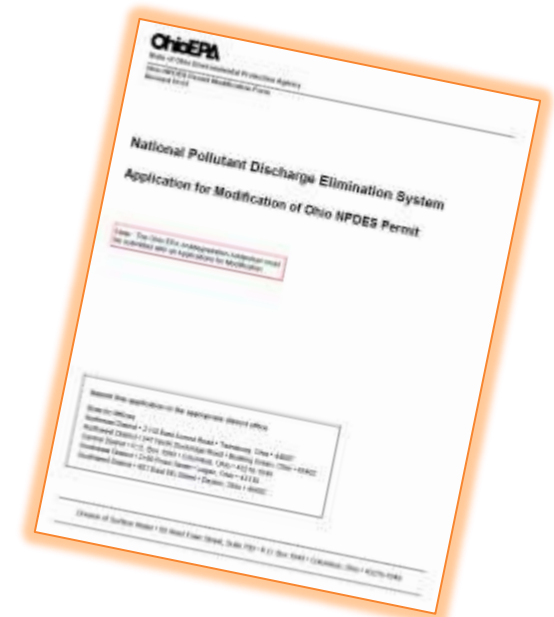
- 1-yr post study – is data different?

Path forth:

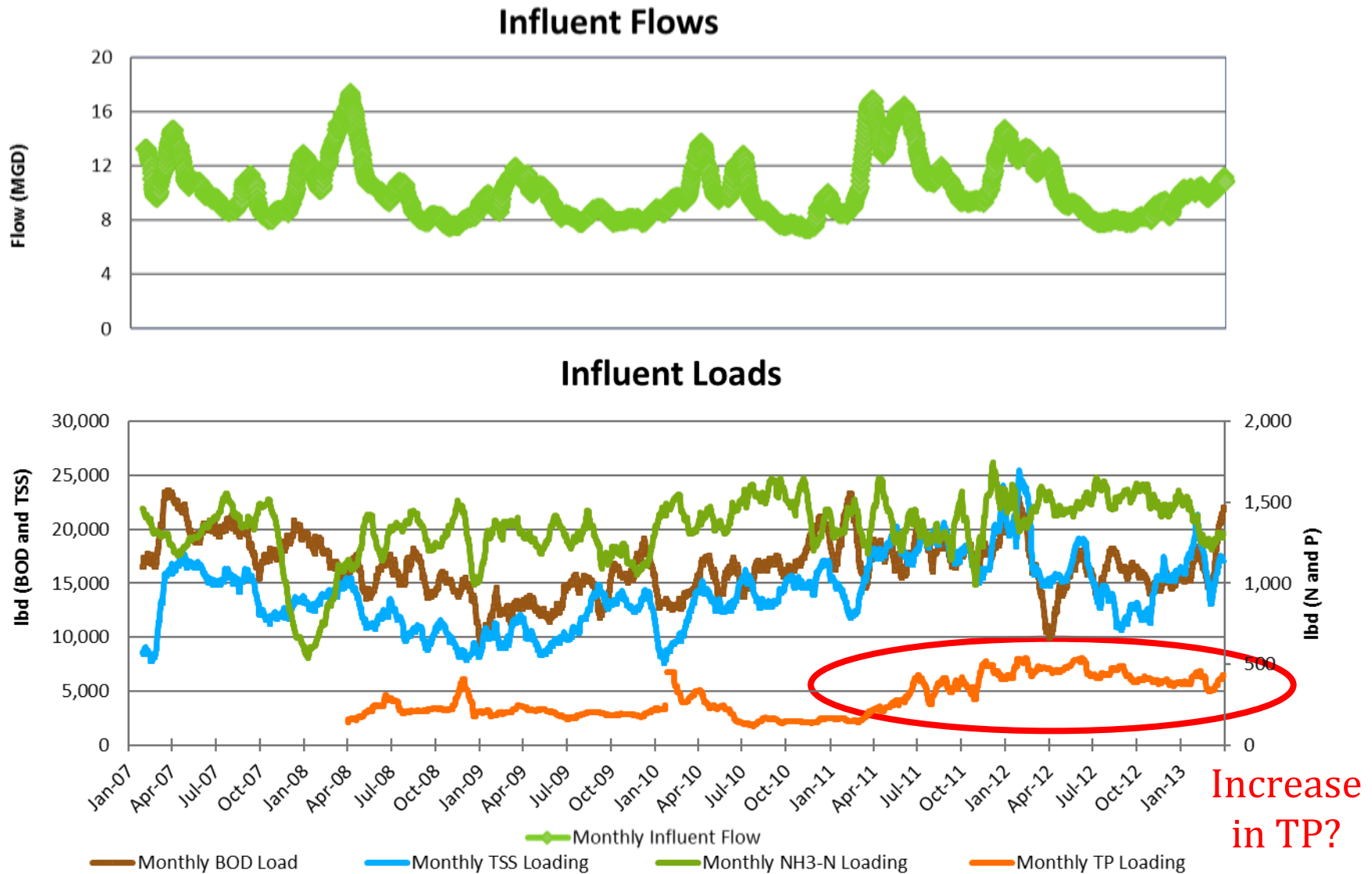
- Request Permit Extension, Evaluate Data, An/Ax Volume

NPDES Permit Schedule Modification Request

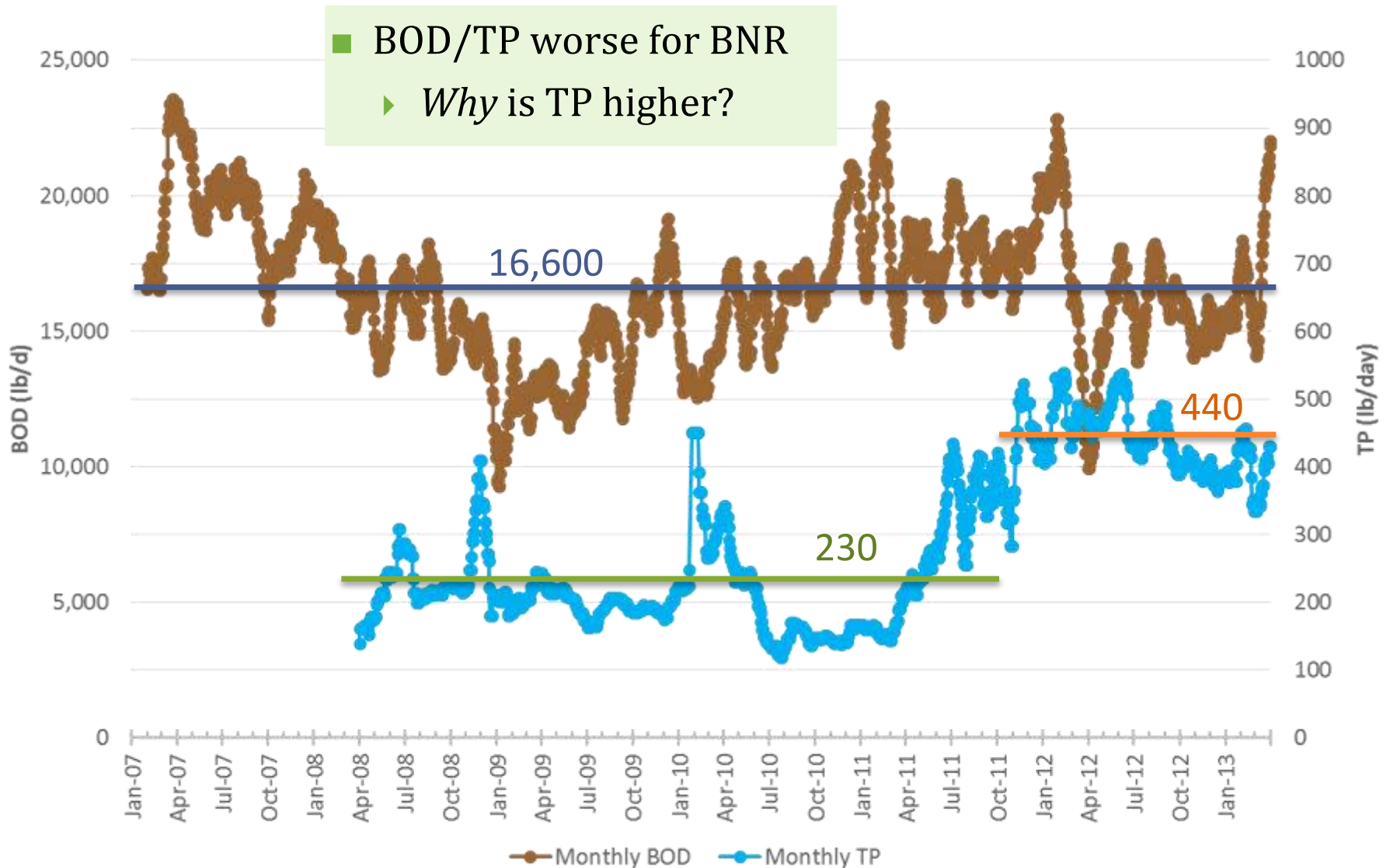
- Additional Time Required to:
 1. Apply and Receive Loan
 - › Water Pollution Control Loan Fund (WPCLF)
 - ▶▶ 0% Interest Loan, \$6 M Savings
 2. Establish Agreement with Stark County
 3. Develop and Detail Scope
 - › Comprehensive plant-wide upgrades
 - ▶▶ Want to best utilize high capital budget
- Requested Extension to NPDES Schedule
 - ▶ Extended 60 to 94 Months
 - › **Meet 1 mg/L TP January 2019**



Evaluation of New Data – Influent Flows and Loads

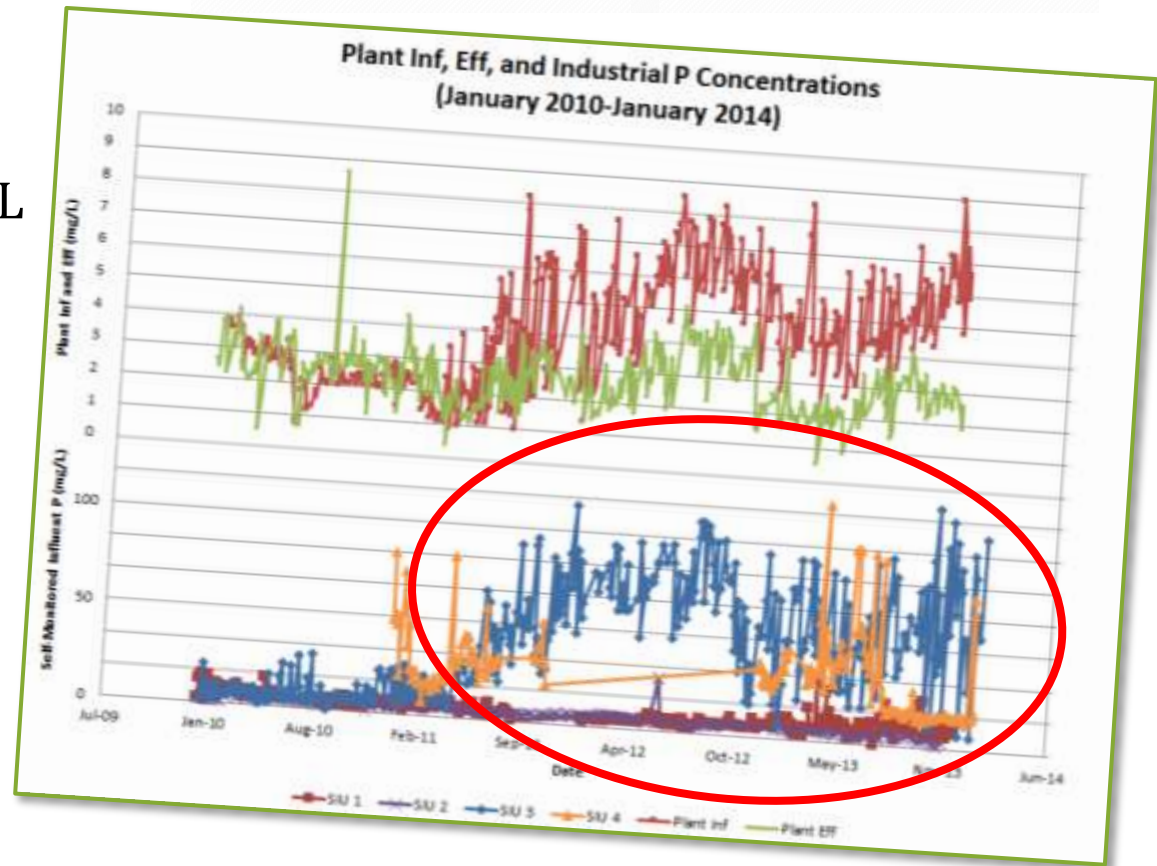


Evaluation of New Data –TP Loads Increased



Increases from Industry

- Industrial TP Increases
 - ▶ Current data
 - ▶ 20 year projections
 - ▶ New expansion
- Design TP
 - ▶ 3.6 mg/L → 4.7 mg/L
 - ▶ +160 lbd @ 17 MGD
- Design BOD/TP
 - ▶ Reduced 24%



Industrial

Limit TP

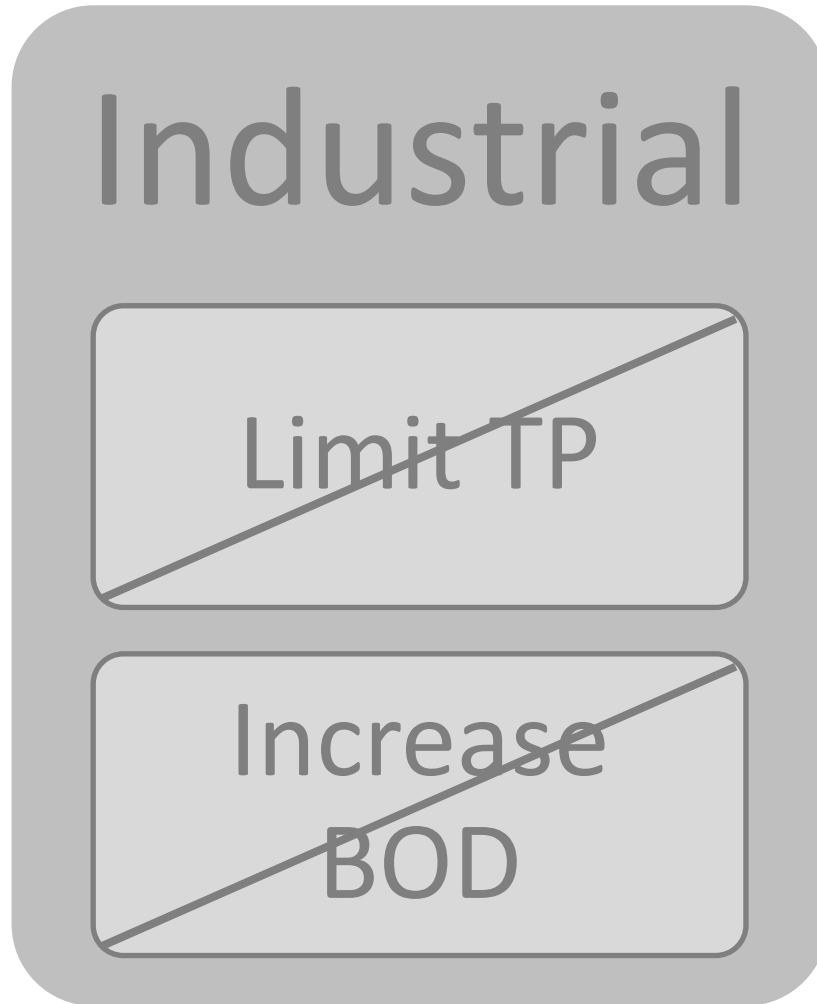
Increase
BOD

In Plant

Increase
An/Ax

Side-stream
loads

Evaluating Industrial TP Solutions



- Industrial Limits - Hard Politically
 - ▶ Industry brings jobs, \$
 - › Example Expansion
 - ▶ Rather not limit TP further
- Models suggest 270 mg/L Inf BOD required for adequate NR
 - ▶ 1.5x Current (180 mg/L)
 - ▶ Another Political issue
 - › Hard to enforce
 - ▶ Hard to ensure consistency

In Plant

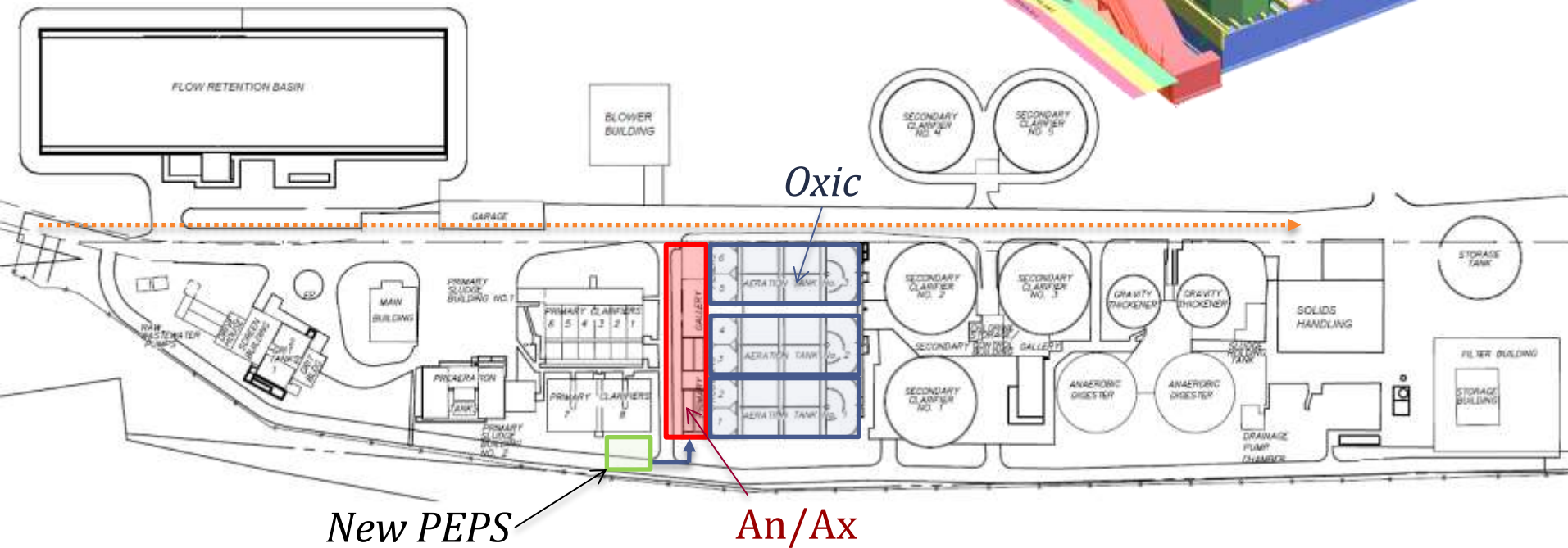
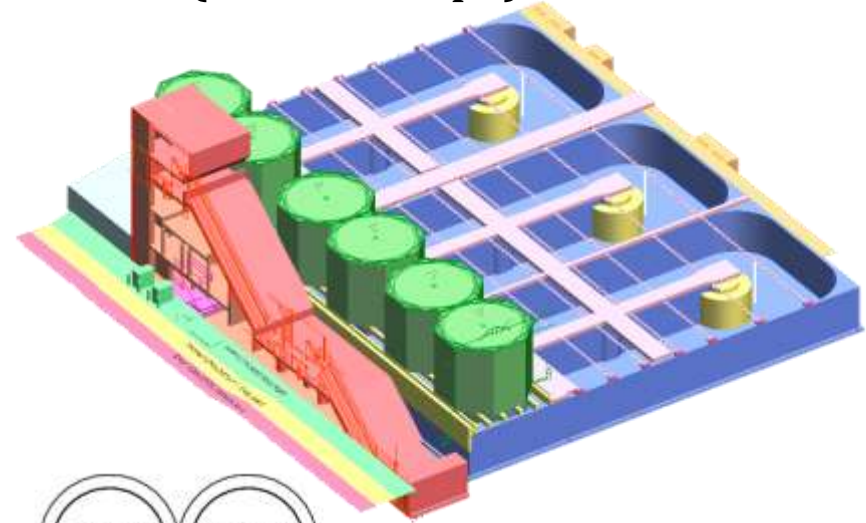
Increase
An/Ax

Side-stream
loads

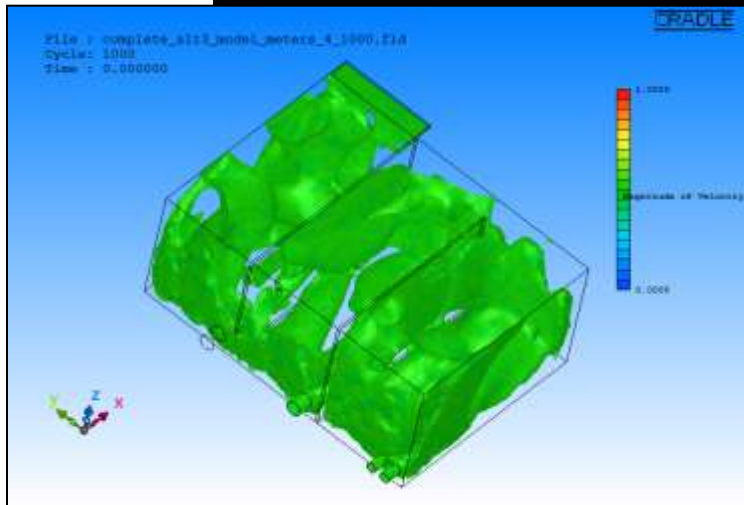
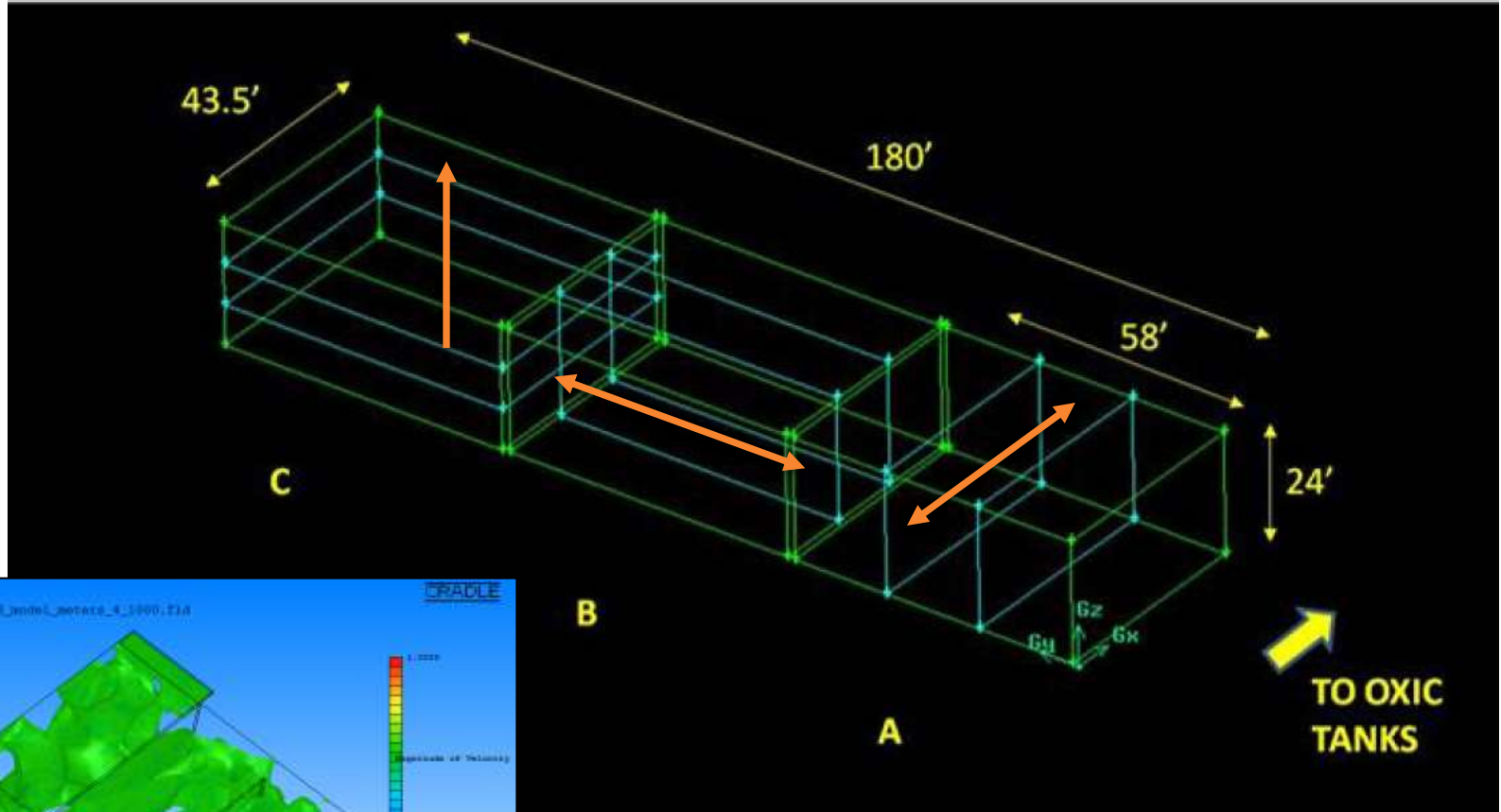
- City prefers In Plant Solutions
- Evaluating Options:
 - › How and Where?
 - ▶▶ (Ex. Footprint)
 - › Maintain Project Goals?
 - ▶▶ (Ex. Footprint)
 - › Minimize Budget Increases?
 - ▶▶ (Above the \$2 M for TN)

Increase An/Ax – “Chimney”

- Demolishing screw pumps → New smaller PEPS (VTSH Pumps)
 - ▶ Deep An/Ax tanks before Oxidic
 - › 24 ft SWD
 - ▶▶ CFD Model Flow Path



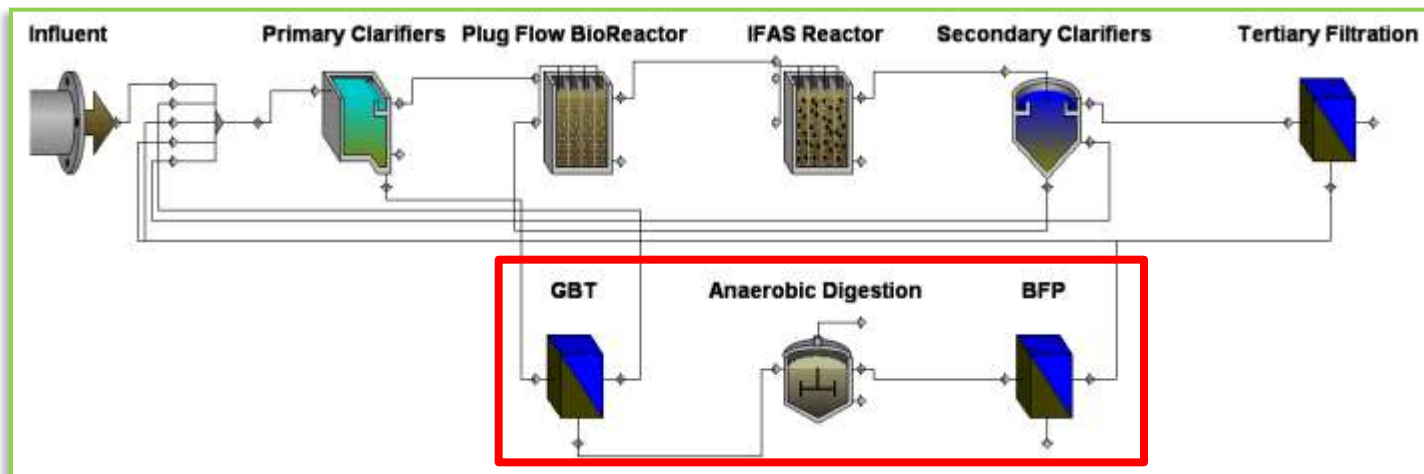
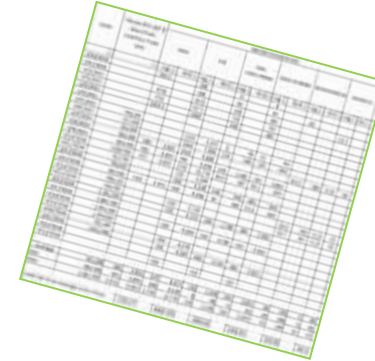
Increase An/Ax – “Chimney” – CFD Results



- 3 Trains, Split to 3 Zones
 - ▶ An – An/Ax Swing - Ax
- 3 Options: “A” predicted best mixing

Side-stream Loads – How and Where?

- Model results suggest high nutrient loads in solids handling recycles
 - ▶ 1,200 mg/L OP - Real?
- Initial Filtrate Special Sampling Results:
 - ▶ Concentrations lower than expected
 - › (Combined 10-20 mg/L OP)
 - ▶ However, total load (300 lbd) 2x Increase in Influent TP (160 lbd)
 - › *Could side-stream removal significantly reduce TP load to IFAS?*



Side-stream Loads – How and Where?

- ▶ Limited budget for side-stream treatments (Ostara, Anita Mox)
 - › Coagulant addition? Ex. Ferric Feed System (odors)

1-2 Dedicated Primary Clarifiers?

Treat side-streams together

But, limited SOR

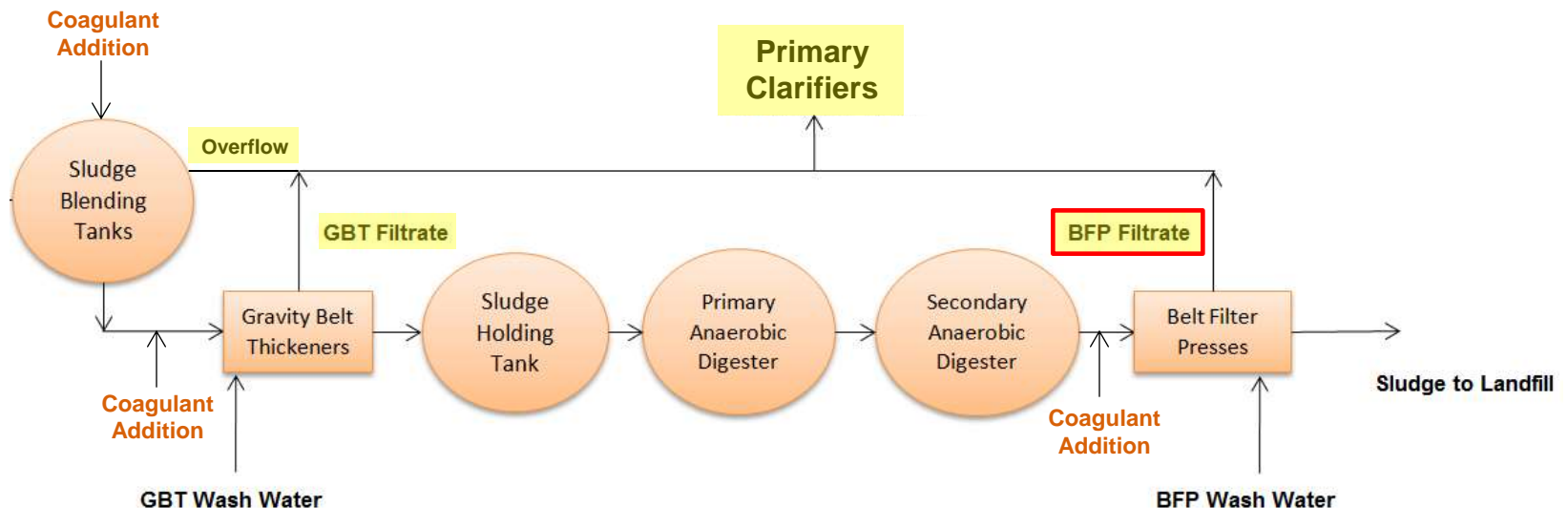
Primary Activation

Addition Direct to Source?

System Already in Place

BFP Most Concentrated (post – AD)

Perform full scale test?



Side-stream Loads – 2nd Special Sampling and Testing

■ Second Round of Sampling to:

1. Test Increasing Ferric Feed

- ▶ To BFPs to evaluate side-stream OP removal

2. Further Evaluate Influent and Sidestream Characterization

- ▶ Confirm high nutrient loads ($\text{NH}_3\text{-N}$, OP)

3. (Bonus!) Evaluate Struvite ($\text{MgNH}_4\text{PO}_4 \cdot 6\text{H}_2\text{O}$)

- ▶ City had mentioned struvite issue on GBT and BFP belts
- ▶ Struvite scale typical post-digestion
 - › 2 constituents are nutrients of interest
 - › Could coagulant addition affect production?



Side-stream Loads – 2nd Special Sampling Procedure

■ Basic Procedure:

- ▶ Sample nutrients and struvite parameters for baseline (3x)
- ▶ Ramp up Ferric feed to BFPs

■ Streams to test

- ▶ Plant Influent
- ▶ GBT Influent*
- ▶ BFP Influent*

■ Parameters to Test (3x)



Filtered (soluble):	Ortho-Phosphorus (OP)	Ammonia (NH ₃ -N)	Dissolved Magnesium (Mg)
Unfiltered (total):	Phosphorus (TP)	Nitrogen (TN)	Magnesium (Mg)
Specific Conductance			

**Filtrates were tested in the first round of sampling*

Side-stream Loads – 2nd Special Sampling – Ferric Feed Test

- Following the third baseline sample:
 - ▶ While dewatering (8 hours)
 - ▶ Increase Ferric feed every two hours
 - › to ~10x current feed rate
 - ▶ Sample OP in Filtrate every two hours



Hour of Test	Ferric Feed Rate (gpm)
1	10
3	40
5	70
7	96

Side-stream Loads – 2nd Special Sampling - Average Results

Flow Stream	TP	OP	NH ₃ -N	TKN as N	Magnesium	Dissolved Magnesium	Conductivity
	mg/L						uS/cm
Plant Inf	4.66	1.51			23.9	18.9	1047
GBT Inf	323	127	218	2375	43.0	6.9	2249
BFP Inf	977	361	1782	2440	122	28.4	4367

- Average Plant Influent TP around estimated design value (4.7 mg/L)
 - ▶ Range 3.4 – 5.4 mg/L
- Inf GBT, BFP OP >> than previous Filtrate sampling (Combined 10-20 mg/L)
 - ▶ Suggests existing ferric feed operations already removing OP

Side-stream Loads – 2nd Special Sampling -Struvite Analysis

Struvite Tool Results						
	Flow	Struvite Predicted?	Struvite Produced	Total Mg	NH ₃ -N	OP
Flow Stream	m ³ /day	% of 4 Tests	kg/day	mg/L		
Inf GBT	940	25%	16	43	218	127
Inf BFP	195	100%	225	8	1716	215

*Note pH and Temp Estimated at 7 and 25 deg C

■ Calculating Struvite Precipitation Potential

- ▶ Sacramento State - Office of Water Programs Tool (\$75)
 - › Excel Based Software



■ Input Measured Influent Data (Mg, NH₃-N, OP, Specific Conductance, Flow)

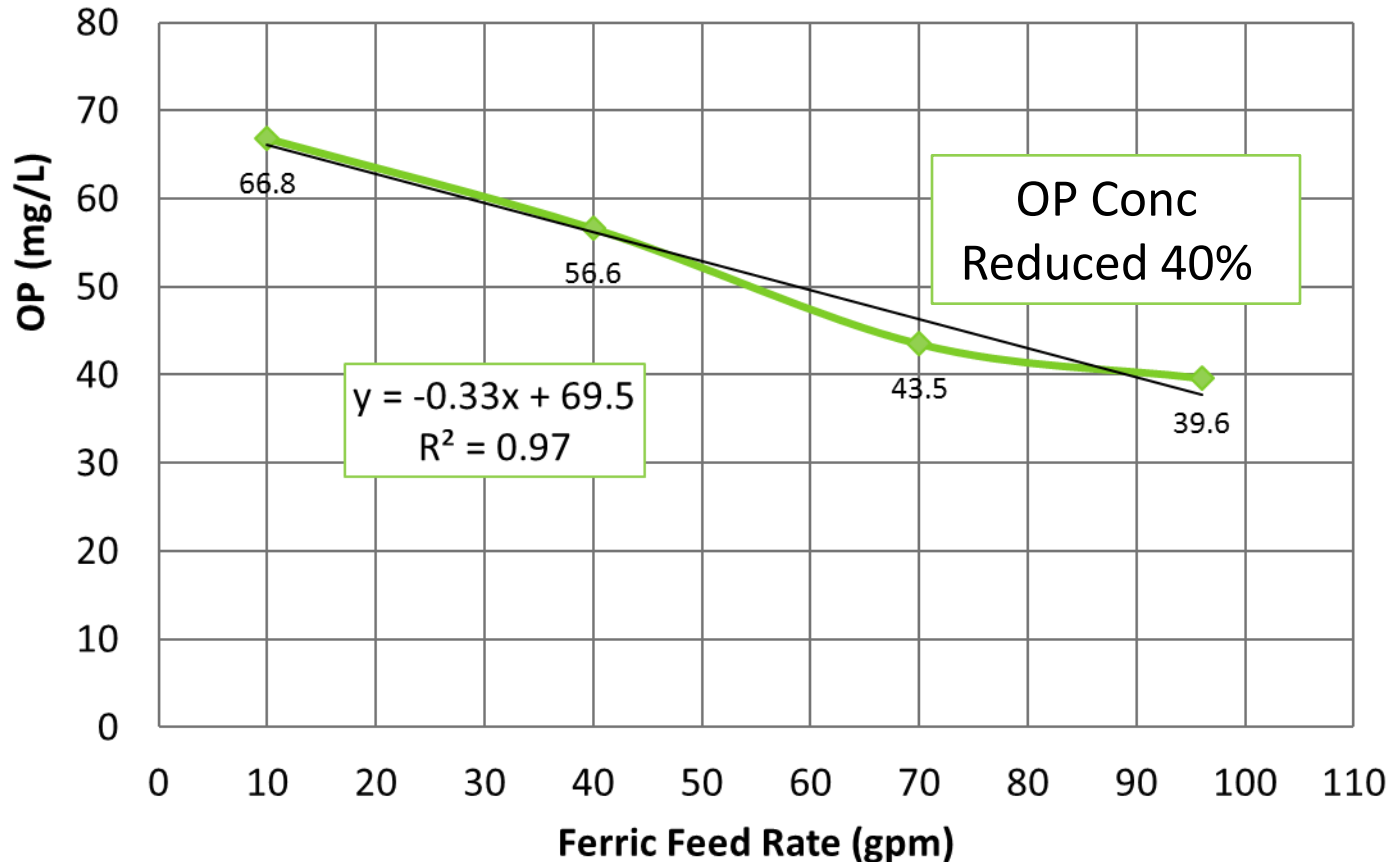
- ▶ Following Expectations:
 - › BFPs have larger Precipitation Potential
 - › OP Decreases with Struvite Production (361 → 215 mg/L in BFP)

■ California WEA Presentation “Dealing with Struvite” (Buhrmaster and Abraham 2011)

- ▶ <http://www.owp.csus.edu/courses/additional/struvite-precipitation-potential-calculation-tool.php>

Side-stream Loads – 2nd Special Sampling- Ferric Test Results

BFP Filtrate Ferric Feed Test Results



- Strong linear response – OP decreases with Ferric feed
 - ▶ *No visual changes to struvite production*

Side-stream Loads - Summary and Assumptions for Final Design

■ Summary of Special Sampling

- ▶ Nutrient loads confirmed
 - › Inf BFP and GBT OP >> than Filtrate (1st Round)
 - ▶▶ Ferric feed already reducing OP?
- ▶ Increased Ferric feed can decrease Filtrate OP
 - › By 40% with ex. pump max
- ▶ BFP more struvite potential
 - › but no noticed change during test

■ For Final Design:

- ▶ Assume 50% removal of OP in BFP Filtrate with increased Ferric
 - › 5% at other side-streams
- ▶ City already planning to upgrade Ferric feed pumps
 - › Will acquire larger pump



At 30% Design:

An/Ax Volumes Increased

- Minimal Additional Footprint

Side-stream Treatment

- Minimal Additional Project Budget

Industry not affected

- Ex. Industrial Limits Remain

New Challenge:

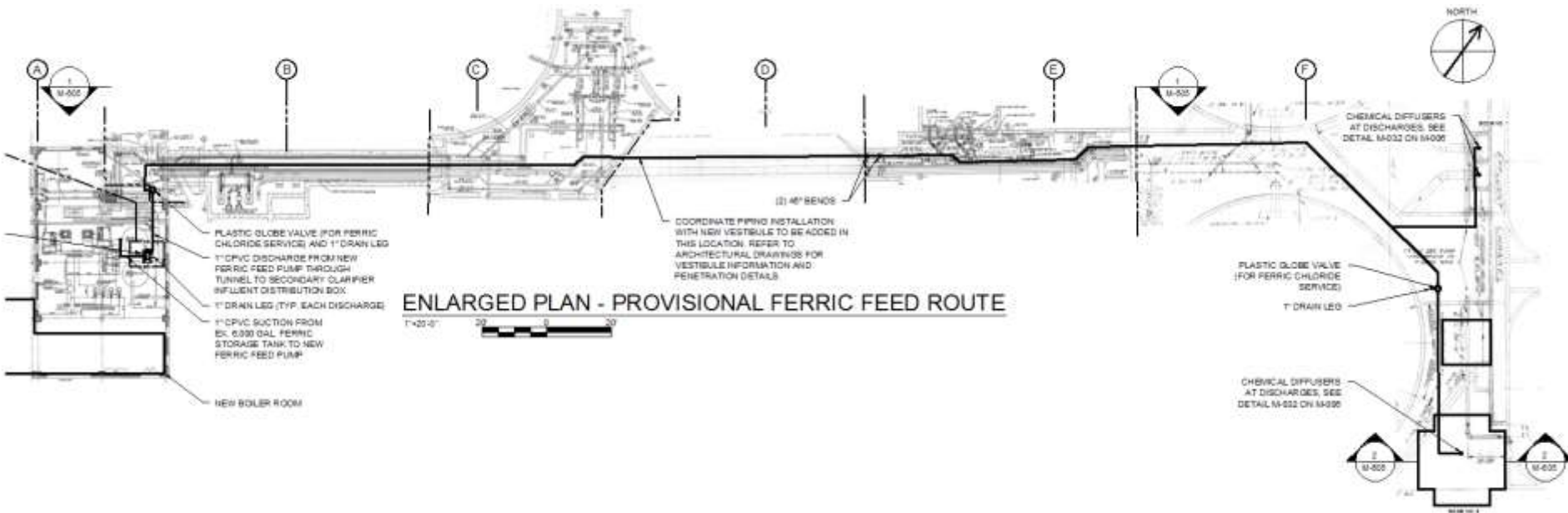
Tertiary Filter Vendors:

Performance Guarantee?

Concerned with Filter Inf TP

Tertiary Filter TP Concerns – Add Provisional feed

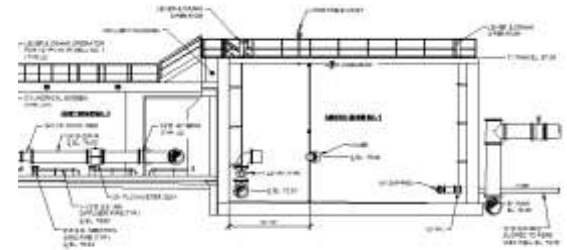
- Goal for all Bio-P (Normal Operations)
- Need to Link Bio + Tertiary Performance Guarantees
 - ▶ Ensure Permit Compliance
- Add provisional chemical feed to Secondary Clarifier Influent



Summary of Challenges and Solutions

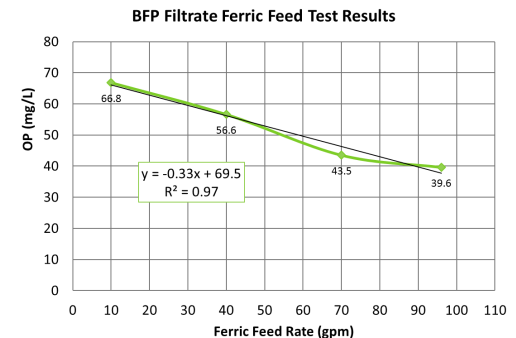
■ Challenges to accommodating Industrial Nutrient Loads:

- ▶ Potential Future Limits
 - Acknowledging pending OEPA NR Strategies
- ▶ Potential Changes in Loads
 - New expansions could increase loads, worsen ratios
- ▶ Political Boundaries
 - Industry brings revenue to City
- ▶ Budgetary Constraints



■ Navigating Solutions

- ▶ Balancing act for both N and P in limited footprint
- ▶ Evaluate available resources
 - Non-traditional tank geometry to fit into site
 - Existing Ferric feed system
 - *Minimal additional footprint & budget required*



THANK YOU



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QUESTIONS?

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